

# INNOVATIVE DESIGN OF PHOTOELECTROCHEMICAL CELLS FOR WATER SPLITTING: SCALE-UP THROUGH NUMBERING-UP AND INTEGRATION INTO A PANEL

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#### **FOTOH2 CONCEPT**

**FotoH2** shall develop a highly efficient <u>tandem photoelectrolysis</u> cell and PANEL for solar H<sub>2</sub> production, based on **durable** and **cost-effective** advanced materials and interfaces. The following specific breakthroughs are targeted:

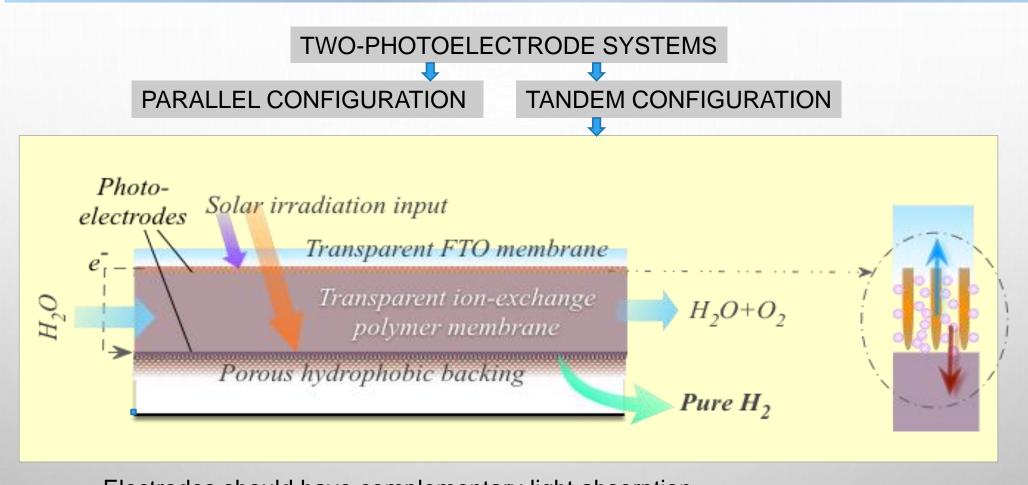
- > Developing cost-effective advanced photoelectrode materials
- > Achieving long-lasting cells for solar H<sub>2</sub> production
- ➤ Simple flow-cell design
- > INPUT: PURE WATER
- > Production of pure H<sub>2</sub> in the output stream
- ➤ High Solar-to-Hydrogen conversion efficiency







#### **FOTOH2 CONCEPT**





Electrodes should have complementary light absorption

Electrolyte should have minimum light absorption and resistance

Separator should avoid crossover of the electrolysis products

Good scalability: flat configuration

PEMs



#### **ELECTRODE MATERIALS**

#### PHOTOELECTRODE REQUERIMENTS

- ☐ Narrow band gap (efficient light absorption).
- ☐ Adequate **band edge locations** for water reduction and oxidation reactions.
- ☐ High **chemical stability** in the dark and under illumination.
- ☐ Good charge transport across the semiconductor bulk.
- ☐ Low overpotentials for water oxidation and reduction reactions.

#### For the viability of a practical device:

- ☐ Low cost reagents for electrode synthesis.
- ☐ Low cost and scalable synthesis route.
- ☐ Materials composed of Earth abundant elements.
- ☐ Non-toxic and environmental friendly materials.









#### **ELECTRODE MATERIALS**

#### 1st PEC cell

1972

# Fujishima and Honda cell

### Electrochemical Photolysis of Water at a Semiconductor Electrode

ALTHOUGH the possibility of water photolysis has been investigated by many workers, a useful method has only now been developed. Because water is transparent to visible light it cannot be decomposed directly, but only by radiation with wavelengths shorter than 190 nm (ref. 1).

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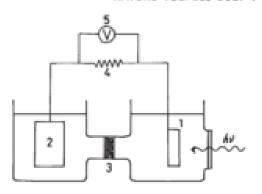
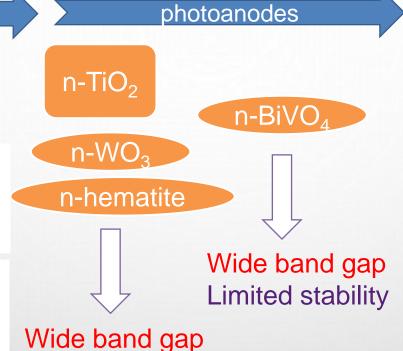
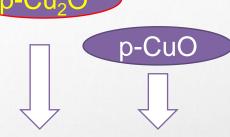


Fig. 2 Electrochemical cell in which the TiO<sub>2</sub> electrode is connected with a platinum electrode (see text). The surface area of the platinum black electrode used was approximately 30 cm<sup>2</sup>.



High stability

photocathodes

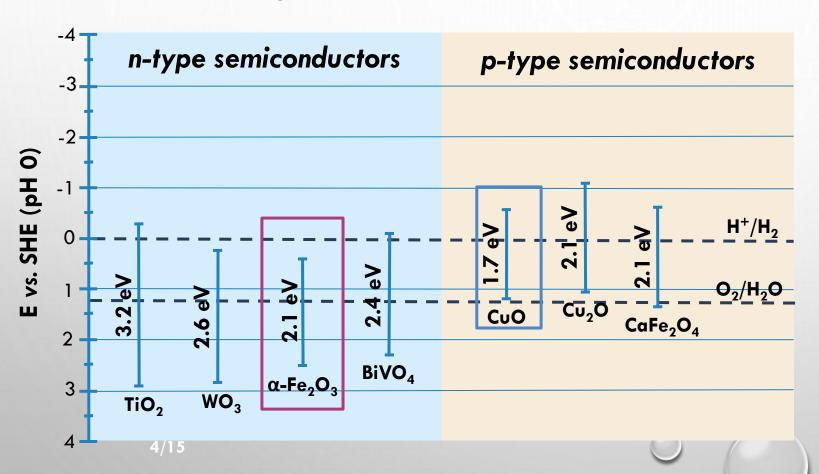


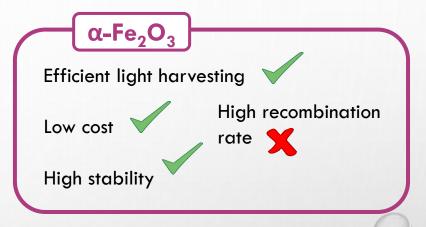
High photocurrents
Narrow band gap
Low stability

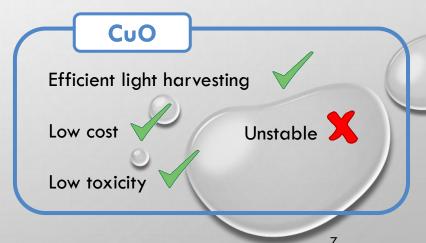




> Among all the potential candidates, which to choose?





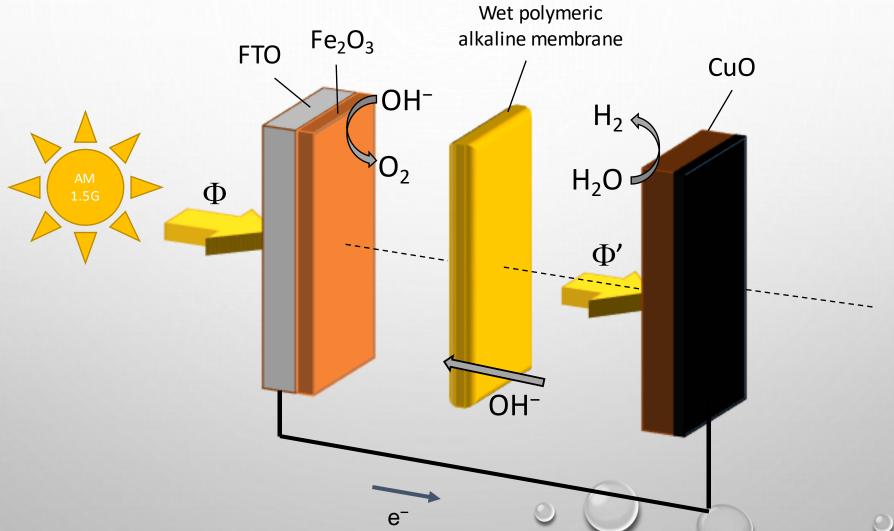








#### Theoretical validation of the FOTOH2 concept

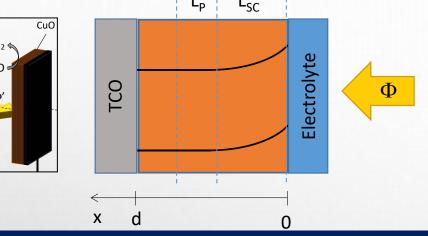




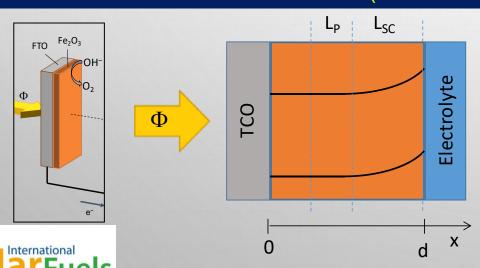




#### MODEL FOR **FRONT** ILLUMINATION (PHOTOCATHODE)



#### MODEL FOR **BACK** ILLUMINATION (PHOTOANODE)

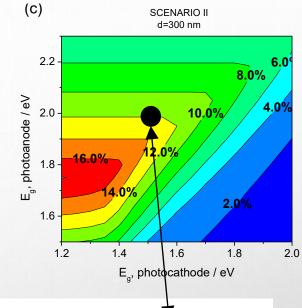


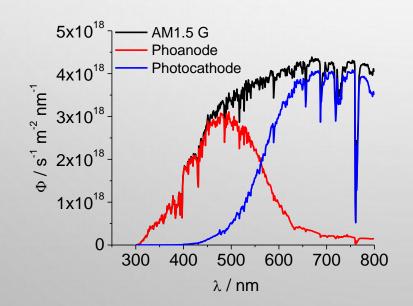
# IMPROVEMENTS RESPECT TO THE ORIGINAL GÄRTNER MODEL:

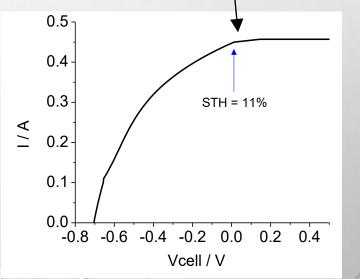
- a) Polychromatic light: AM 1.5G (instead of monochromatic light)
- b) Kinetic model (recombination and charge transfer rate constants)
- c) Absorption coefficients as a function of the wavelength (Tauc relationships)

#### **TANDEM CELL: HEMATITE-CuO**

PHOTOANODE		PHOTOCATHODE		MEMBRANE	
E <sub>fb</sub> / V vs RHE	0.3	$E_{\rm fb}$ / V vs RHE	1	$\sigma$ / S cm $^{ extsf{-}1}$	0.1
$\mathcal{E}_{hem}$	80	$\epsilon_{C_{U}O}$	115	L $/~\mu$ m	50
L <sub>p</sub> / nm	5	$L_{n}  /  nm$	50	$A \ / \ cm^2$	50
A / cm <sup>2</sup>	50	$A / cm^2$	50		
$N_{\rm D}$ / cm <sup>-3</sup>	10 <sup>17</sup>	$N_A / cm^{-3}$	10 <sup>17</sup>	R ( $\Omega$ )	0.001
d / mm	0.150	d / mm	2		

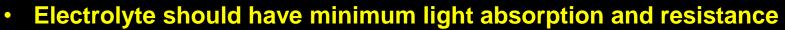












- Separator should avoid crossover of the electrolysis products
- Good scalability: flat configuration



# POLYMER ELECTROLYTE MEMBRANE

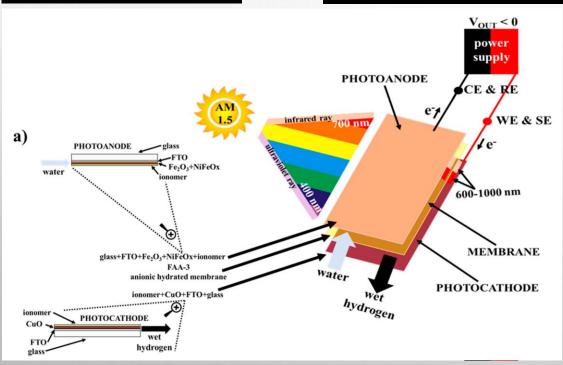
# FTO-SUPPORTED PHOTOCATHODE

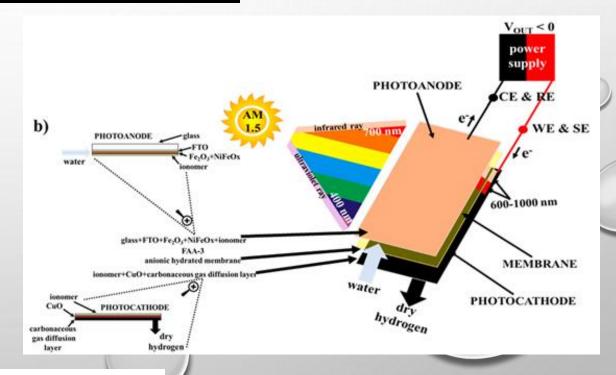


PHOTOCATHODE SUPPORTED ON CARBONACEOUS GAS DIFFUSION LAYER



#### **DRY HYDROGEN**

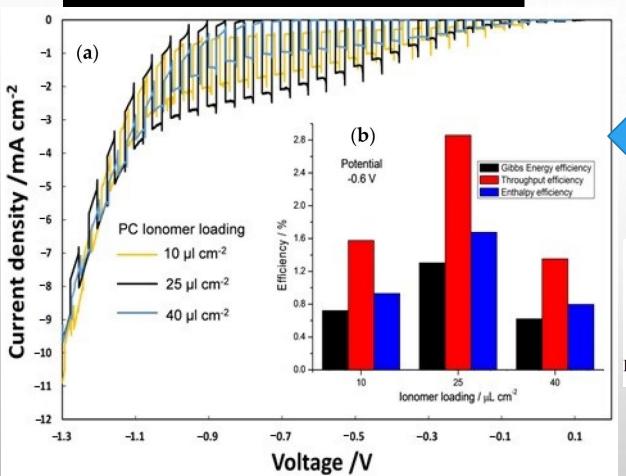








#### MEMBRANE ELECTRODE ASSEMBLY



- Fumasep membrane (FAA3-50 from Fumatech)
- Thickness of 50 µm
- Based on a brominated polysulfone backbone with quaternary ammonium side chain groups

#### EFFECT OF THE IONOMER DISPERSION LOADING

Enthalpy efficiency  $\eta_{Enth} = I_p \; (\Delta H/nF - E_{bias})/P_{in} = I_p \; (E_{tn} - E_{bias})/P_{in}$ 

Gibbs Energy efficiency  $\eta = I_p \; (\Delta G/nF - E_{bias})/P_{in} = I_p \; (E_{rev} - E_{bias})/P_{in}$ 

Throughput efficiency  $\eta_{throughput} = I_p (\Delta H/nF)/(P_{in} + I_p E_{bias}) = I_p E_{tn}/(P_{in} + I_p E_{bias})$ 

 $E_{tn} = 1.48 \text{ V}$ ,  $E_{rev} = 1.23 \text{ V}$ ,  $E_{bias} \equiv V$ ,  $P_{in} \equiv mW \text{ cm}^{-2}$  and  $I_p = I_{light} - I_{dark} \equiv mA \text{ cm}^{-2}$ .



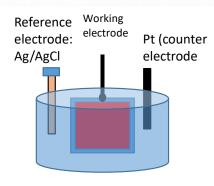


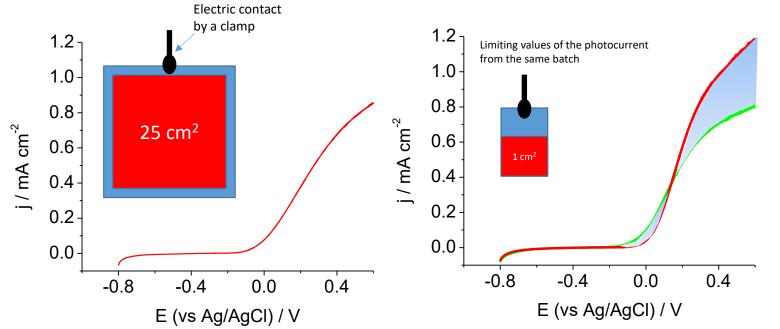




#### **TOWARDS A PANEL**

EFFECT OF THE FTO CONDUCTIVITY IN THE 25 cm<sup>2</sup> HEMATITE PHOTOANODE





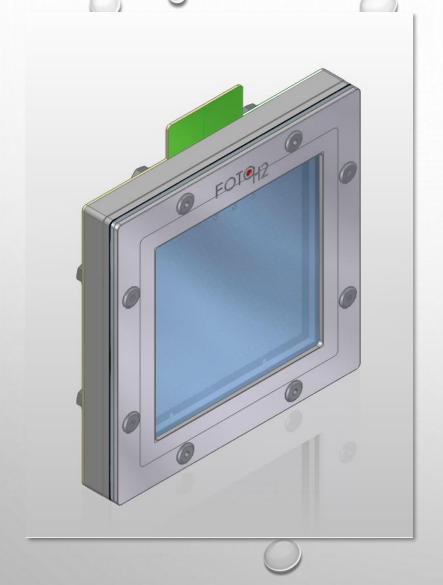


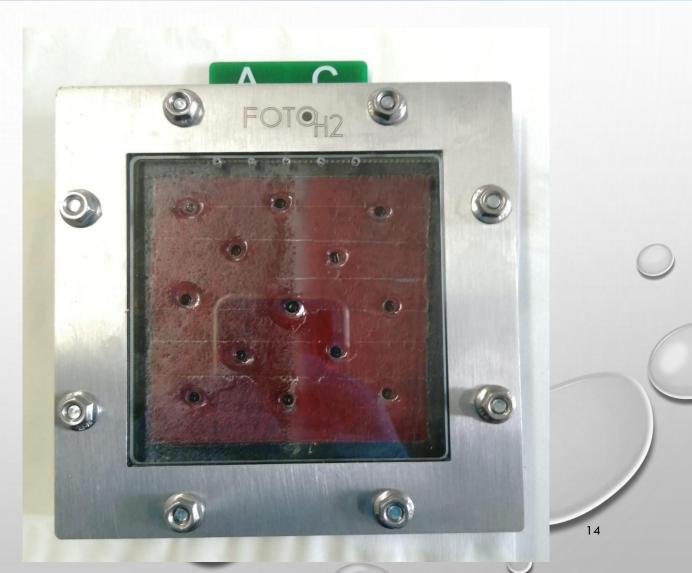
Conductivity of the glass is not the main limitation of the photocurrent.





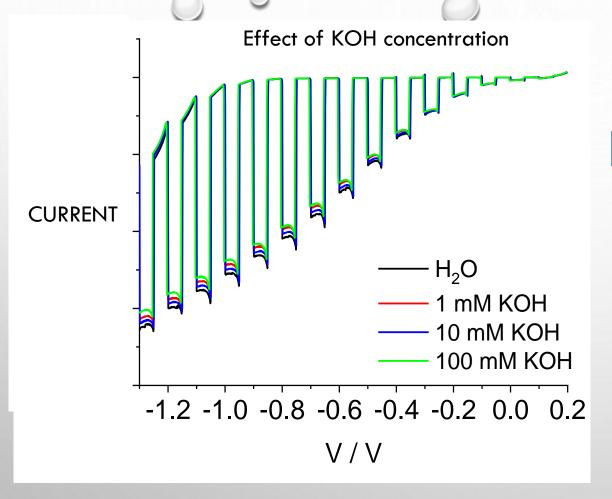
### **SCALING-UP THE PEC CELL**

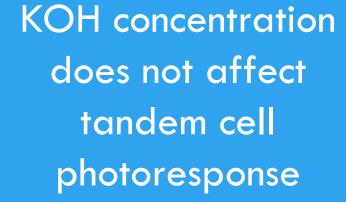






### **SCALING-UP THE PEC CELL**







All measurements in this presentation are done in  $N_2$ -purged water







# 2

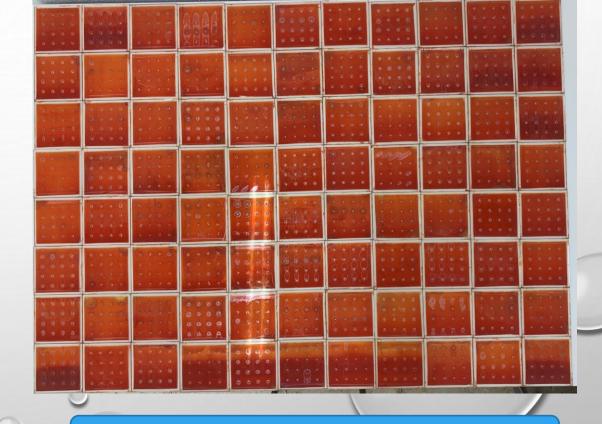
#### **TOWARDS A PANEL**

Up to 4 electrodes at once

Up to 8 electrodes at once







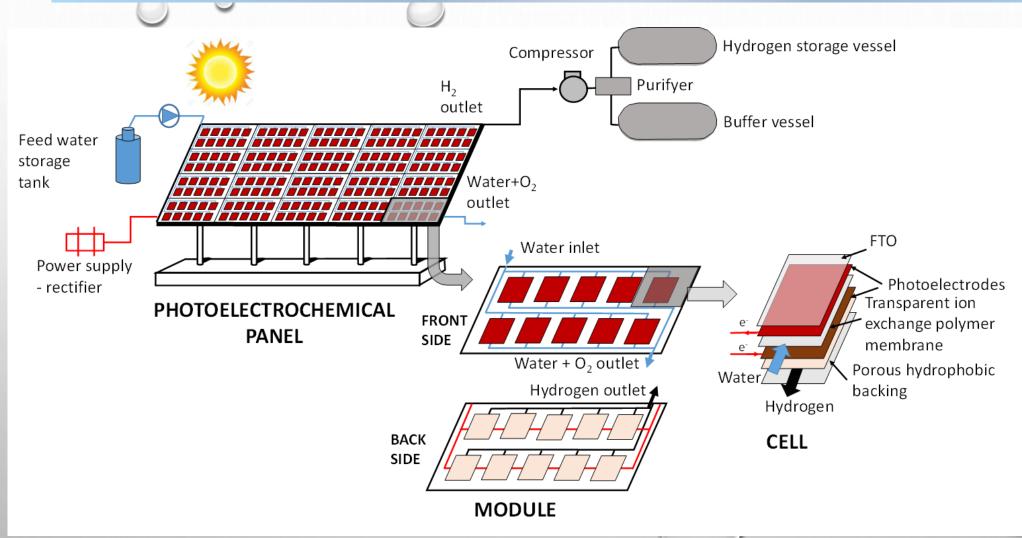
First reactor design

Final reactor design





#### **TOWARDS A PANEL**



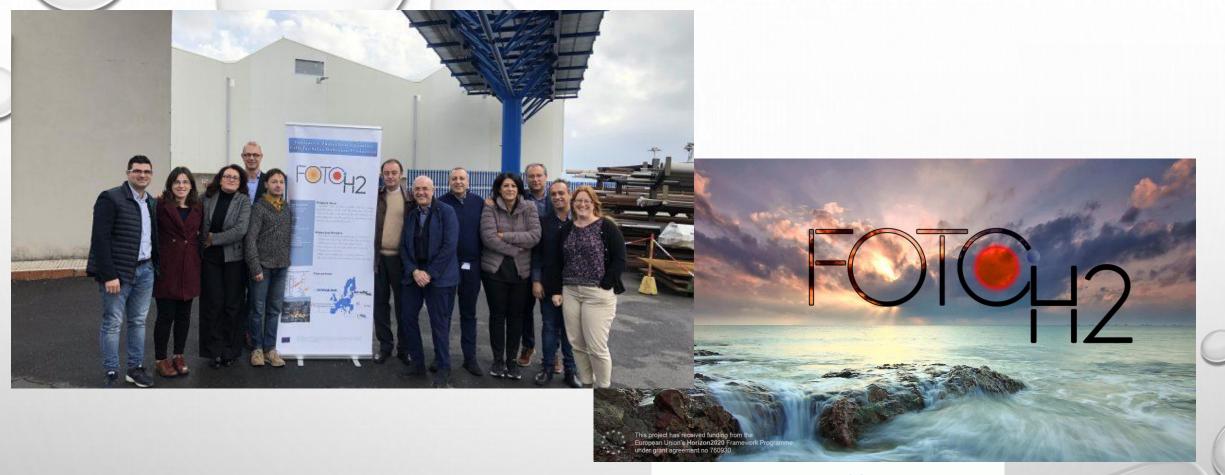






- > EFFICIENT OXIDE/POLYMER ELECTROLYTE MEMBRANE CONFIGURATION
- > GOOD SCALABILITY OF HEMATITE ELECTRODES
- >INTERFACE PHOTOELECTRODE/PEM DESIGNED FOR MINIMIZING CHARGE TRANSFER RESISTANCE
- > FLAT CELL CONFIGURATION FED WITH WATER
- > NOVEL CELL, MODULE AND ANCILLARY EQUIPMENT DESIGN





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